

**GUJARAT TECHNOLOGICAL UNIVERSITY****BE- SEMESTER-IV (NEW) EXAMINATION – WINTER 2020****Subject Code:3140507****Date:24/02/2021****Subject Name:Chemical Engineering Thermodynamics II****Time:02:30 PM TO 04:30 PM****Total Marks:56****Instructions:**

1. Attempt any FOUR questions out of EIGHT questions.
2. Make suitable assumptions wherever necessary.
3. Figures to the right indicate full marks.

- Q.1** (a) Write down Raoult's law and Henry's law explaining each term associated with them with their applicability. **03**
- (b) Write a brief note on retrograde condensation and its application. **04**
- (c) Define azeotrope and explain the minimum boiling and maximum boiling azeotropes with suitable examples. **07**
- Q.2** (a) Discuss the phase rule and Duhem's theorem. **03**
- (b) At 303 K, vapour pressures of benzene (1) and toluene (2) are 15.75 kPa and 4.89 kPa respectively. Determine the partial pressure and composition of the benzene vapour in equilibrium with a liquid mixture consisting of equal weight of the two components. **04**
- (c) Define partial molar properties. Discuss various methods for evaluation of partial molar properties. **07**
- Q.3** (a) Estimate activity coefficient of methanol for chloroform (1) / methanol (2) system at 35°C. The vapour pressures of chloroform and methanol at 35° are 39.54 kPa and 27.95 kPa respectively. The mole fraction of methanol in the liquid mixture is 0.25. Margules' parameters are  $A_{12} = 0.738$ ,  $A_{21} = 1.868$ . **03**
- (b) Discuss the area test for checking the thermodynamic consistency of experimental VLE data. **04**
- (c) The enthalpy at 300 K and 1 bar of a binary liquid mixture is represented by the following equation:  
 $H = 400 X_1 + 600 X_2 + X_1 X_2 (40X_1 + 20X_2)$ , where H is in J/mol. Determine expressions for  $\bar{H}_1$  and  $\bar{H}_2$  as functions of  $X_1$ , numerical values for the pure species enthalpies  $H_1$  and  $H_2$ , and numerical values of partial enthalpies at infinite dilution  $\bar{H}_1^\infty$  and  $\bar{H}_2^\infty$ . **07**
- Q.4** (a) Methanol (1) / acetone (2) system is described by the Van Laar activity coefficient model. At 60°C, the model parameters are  $A_{12} = 0.47$  and  $A_{21} = 0.78$ . Estimate the activity coefficient of methanol for a solution containing 15 mol% of methanol. **03**
- (b) Consider a vessel which initially contains only  $n_0$  moles of water vapor. If decomposition occurs according to the reaction:  $H_2O \rightarrow H_2 + 0.5O_2$ . Find expressions which relate the number of moles and mole fraction of each chemical species to the reaction co-ordinate and fractional decomposition of water vapor. **04**
- (c) Using fundamental property relations, establish the expression of standard Gibbs free energy change of a chemical reaction as a function of the thermodynamic equilibrium constant. **07**
- Q.5** (a) Define K-value and explain its importance in vapour-liquid equilibrium calculations. **03**

- (b) Derive the expression of vapour composition at equilibrium using flash vapourization. **04**  
 (c) Derive the Gibbs – Duhem equation for a binary solution in terms of activity and activity coefficient. **07**
- Q.6** (a) Write a brief note on ideal solutions. **03**  
 (b) Derive the Margules<sup>2</sup> equations from the expression  $\frac{G^E}{x_1x_2RT} = A_{21}x_1 + A_{12}x_2$ . **04**  
 (c) The experimental pressure volume data for benzene at 675 K from a very low pressure to about 75 bar may be approximated by the equation,  $V = 0.0561(1/P - 0.0046)$ , where V is in m<sup>3</sup>/mol and P is in bar. What is fugacity of benzene at 1 bar and 675 K ? **07**
- Q.7** (a) Discuss the Gamma/Phi formulation for vapor-liquid equilibrium. **03**  
 (b) Discuss criteria of chemical reaction equilibrium with neat sketch. **04**  
 (c) The vapour pressures of acetone (1) and acetonitrile (2) can be evaluated by the following Antoine equations: **07**
- $$\ln p_1^{\text{sat}} = 14.5463 - \frac{2940.46}{T - 35.93} \quad \text{and} \quad \ln p_2^{\text{sat}} = 14.2724 - \frac{2945.47}{T - 49.15}$$
- where T in K and  $p_i^{\text{sat}}$  in kPa. Assuming that the solution formed is ideal, calculate:
- $x_1$  and  $y_1$  at 327 K and 65 kPa
  - T and  $y_1$  at 65 kPa and  $x_1 = 0.4$
- Q.8** (a) Discuss about liquid-liquid equilibrium (LLE). **03**  
 (b) Develop expressions for the mole fractions of reacting species as functions of the reaction coordinate for: **04**
- A system initially containing 2 mol of NH<sub>3</sub> & 5 mol of O<sub>2</sub> and undergoing the reaction  
 $4\text{NH}_{3(g)} + 5\text{O}_{2(g)} \rightarrow 4\text{NO}_{(g)} + 6\text{H}_2\text{O}_{(g)}$
  - A system initially containing 3 mol of H<sub>2</sub>S & 5 mol of O<sub>2</sub> and undergoing the reaction  
 $2\text{H}_2\text{S}_{(g)} + 3\text{O}_{2(g)} \rightarrow 2\text{H}_2\text{O}_{(g)} + 2\text{SO}_{2(g)}$
- (c) Explain effect of temperature, pressure and total stoichiometric number on equilibrium constant. **07**

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